LETTERS TO THE EDITORS

COMMENTS ON "HEAT TRANSFER AND PRESSURE DROP IN HORIZONTAL ANNULAR TWO-PHASE TWO-COMPONENT FLOW"

R. H. PLETCHER and H. N. McMANUS, JR., *Int. J. Heat Mass Transfer* 11 (7), 1087-1104 (1968).

IN A RECENT article Pletcher and McManus [l] presented interesting correlations of data for heat transfer during air-water flow in pipes. The line in their Fig. 20 is given almost exactly by

$$
\frac{\hbar}{\phi_L} = 5000 \left\{ X \left(\frac{\dot{W}_a}{\dot{W}_L} \right)^{0.4} \right\}^2.
$$
 (1)

The Martinelli parameter X can be written

$$
X = \left(\frac{\dot{W}_L}{\dot{W}_a}\right)^{0.875} \left(\frac{\rho_a}{\rho_L}\right)^{0.5} \left(\frac{\mu_L}{\mu_a}\right)^{0.125} \tag{2}
$$

where a smooth tube surface is assumed. Substituting equation (2) in (1) gives

$$
\frac{\hbar}{\phi_L} \propto \left(\frac{\mu_L}{\mu_a}\right)^{0.25} \left\{ \left(\frac{\dot{W}_L}{\dot{W}_a}\right)^{0.475} \left(\frac{\rho_a}{\rho_L}\right)^{0.5} \right\}^2
$$

which is approximately proportional to

$$
\left(\frac{\mu_L}{\mu_a}\right)^{0.25} \frac{\dot{W}_L}{\dot{W}_a} \frac{\rho_a}{\rho_L}
$$

i.e. to

$$
\left(\frac{\mu_L}{\mu_a}\right)^{0.25} \frac{Q_L}{Q_a}
$$

where Q_L and Q_a are the volume flowrates of water and air respectively. The writer therefore suggests that plots of \hbar/ϕ_L against Q_L/Q_a or $Q_L/(Q_a + Q_L)$ and \hbar against $Q_L/(Q_a + Q_L)$ Q_L) might give a more meaningful correlation of the data than the type of plots used in Fig. 20.

1. R. H. PLETCHER and H. N. MCMANUS JR., Heat transfer and pressure drop in horizontal annular two-phase twocomponent flow, Int. J. Heat Mass Transfer, 11, 1086-1104 (1968).

D. CHISHOLM

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REJOINDER

CHISHOLM has made an interesting and correct observation concerning the parameter, $X(\dot{W}_a/\dot{W}_b)^{0.4}$, used to correlate data in $\lceil 1 \rceil$ for heat transfer to horizontal annular water-air 100 actually computed according to

flow. For the results in [1], the Martinelli parameter X was actually computed according to
\n
$$
X = \left(\frac{W_L}{W_a}\right)^{0.4} \left(\frac{\rho_a}{\rho_L}\right)^{0.5} \left(\frac{\mu_L}{\mu_a}\right)^{0.125}
$$
\n(1) $\frac{\epsilon}{\epsilon}$

(see [l] for nomenclature) which results from computing the single phase turbulent flow friction factor according to an equation of the form

$$
f \propto \frac{C}{Re^{0.2}}
$$
 (2)

where C is a constant. Thus, the parameter $X(\dot{W}_a/\dot{W}_b)^{0.4}$ can be reduced to

$$
\left(\frac{\mu_L}{\mu_a}\right)^{0.1} \left(\frac{Q_L}{Q_a}\right)^{0.5} \tag{3}
$$

without making the approximation indicated by Chisholm. Q_L and Q_a are the volume flow rates of water and air res-
pectively.
efficients from [1] based on O_1/O_1 .

efficients from [1] based on Q_L/Q_a .

Since $(\mu_L/\mu_a)^{0.1}$ was relatively constant over the range of was generally less than one per cent for the data of [1]. Less the data, the ratio of the maximum to minimum value being spread of the data is obtained by plo about 1.1 , it is expected that a reasonably good correlation of the data would be obtained by using $(Q_L/Q_a)^{0.5}$ or (Q_L/Q_a) as a parameter. Figure 1 shows the data in Fig. 20 of (L) \mathbb{Z}_a) 1. R. H. PLETCHER and H. N. MCMANUS, JR., Heat transfer
as a parameter. Figure 1 shows the data in Fig. 20 of [1] and pressure drop in horizontal annul plotted according to \hbar/Q_L vs. Q_L/Q_a as suggested by Chis-
holm. The authors consider Q_1/Q_1 to be an equivalent and component flow, Int. J. Heat Mass Transfer 11, 1087– holm. The authors consider Q_L/Q_a to be an equivalent and component for the necessary $R(W/W)^{0.4}$ for 1104 (1968). perhaps more convenient parameter than $X(\hat{W}_a/\hat{W}_b)^{0.4}$ for correlating the data of $\lceil 1 \rceil$ but they see no physical basis for considering it a more "meaningful" parameter as suggested R. H. PLETCHER* Chisholm. Experiments involving a variety of substances in H. N. MCMANUS, JR.⁺ addition to water and air would be required to determine the true dependence of \bar{h} upon μ_I/μ_a . The authors gave the true dependence of *n* upon μ_L/μ_a . The authors gave μ_B ***** *Department of Mechanical Engineering special attention to the possible use of X as a heat transfer <i>Iowa State University* correlating parameter since pressure drop data has been *Iowa State University*
expected with X for many two-phase systems *Ames, Iowa 50010, U.S.A.* successfully correlated with X for many two-phase systems *Ames, Iowa 50010, U.S.A.*
other than water and air. Regarding some of Chisholm's [†] Sibley School of Mechanical Engineering other than water and air. Regarding some of Chisholm's $\frac{1}{2}$ *Sibley School of M*
other suggeststions $Q_1/(Q_1 + Q_2)$ is nearly equivalent to Cornell University other suggeststions, $Q_L/(Q_a + Q_L)$ is nearly equivalent to *Cornell University* Q_t/Q , since Q_t/Q , is small for annular flows in general and *Ithaca, New York* 14850, U.S.A. Q_L/Q_a since Q_L/Q_a is small for annular flows in general and

spread of the data is obtained by plotting \hbar/ϕ_L rather than \hbar so the former is preferred.

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